

# Influence of various shapes of nanoparticles on unsteady stagnation-point flow of Cu–H<sub>2</sub>O nanofluid on a flat surface in a porous medium: A stability analysis

Astick Banerjee<sup>1</sup>, Krishnendu Bhattacharyya<sup>2,†</sup>, Sanat Kumar Mahato<sup>1</sup>, and Ali J. Chamkha<sup>3</sup>

<sup>1</sup>Department of Mathematics, Sidho-Kanho-Birsha University, Purulia 723104, India

<sup>2</sup>Department of Mathematics, Institute of Science, Banaras Hindu University, Varanasi 221005, India

<sup>3</sup>Faculty of Engineering, Kuwait College of Science and Technology, Doha District, Kuwait

(Received 13 May 2021; revised manuscript received 15 July 2021; accepted manuscript online 1 September 2021)

The nanofluid and porous medium together are able to fulfill the requirement of high cooling rate in many engineering problems. So, here the impact of various shapes of nanoparticles on unsteady stagnation-point flow of Cu–H<sub>2</sub>O nanofluid on a flat surface in a porous medium is examined. Moreover, the thermal radiation and viscous dissipation effects are considered. The governing problems of partial differential equations are converted into self-similar coupled ordinary differential equations and those are numerically solved by the shooting method. The computed results can reveal many vital findings of practical importance. Firstly, dual solutions exist for decelerating unsteady flow and for accelerating unsteady and steady flows, the solution is unique. The presence of nanoparticles affects the existence of dual solution in decelerating unsteady flow only when the medium of the flow is a porous medium. But different shapes of nanoparticles are not disturbing the dual solution existence range, though it has a considerable impact on thermal conductivity of the mixture. Different shapes of nanoparticles act differently to enhance the heat transfer characteristics of the base fluid, i.e., the water here. On the other hand, the existence range of dual solutions becomes wider for a larger permeability parameter related to the porous medium. Regarding the cooling rate of the heated surface, it rises with the permeability parameter, shape factor (related to various shapes of Cu-nanoparticles), and radiation parameter. The surface drag force becomes stronger with the permeability parameter. Also, with growing values of nanoparticle volume fraction, the boundary layer thickness (BLT) increases and the thermal BLT becomes thicker with larger values of shape factor. For decelerating unsteady flow, the nanofluid velocity rises with permeability parameter in the case of upper branch solution and an opposite trend for the lower branch is witnessed. The thermal BLT is thicker with radiation parameter. Due to the existence of dual solutions, a linear stability analysis is made and it is concluded that the upper branch and unique solutions are stable solutions.

**Keywords:** Cu–H<sub>2</sub>O nanofluid, various shapes of nanoparticles, unsteady stagnation-point flow, dual solutions, stability analysis

**PACS:** 47.15.Cb, 47.15.Fe, 44.30.+v

**DOI:** 10.1088/1674-1056/ac229b

## 1. Background of the investigation

The boundary layer flow forms adjacent to the surface on which the fluid flows, so its dynamics and effect are much too important in fluid mechanics. While, the heat transfer in the boundary layer is responsible for cooling the surface and consequently, it is a handy tool for many industries. Now, in this era of science, the ultra-high cooling rate is one of the most crucial requirements of many engineering processes and industries, but the primary limitation is small thermal conductivities of traditional fluids, like, water, oil, ethylene glycol, etc. Previously, solid particles are added in traditional fluids to increase the inherently poor thermal conductivity of those traditional fluids and all efforts are centered on the mixing of micrometer-sized particles, but this approach has some technical shortcomings, such as micro-particles are rapidly deposited as a sediment in fluids, those may block the flow and cause an extra pressure drop. This problem can be settled by adding nanometer-sized particles, called nanoparticles, in aforesaid host fluids and the mixture is known as “nanofluid” pro-

posed by Choi.<sup>[1]</sup> Adding nanoparticles with typical sizes less than 100 nm in host fluids drastically improves many thermal properties, especially, the thermal conductivities of the mixtures, i.e., nanofluids. To describe the motion of a nanofluid two models have been proposed, namely, “two-phase”, and “single-phase” by Buongiorno<sup>[2]</sup> and Tiwari and Das,<sup>[3]</sup> respectively. The Tiwari and Das model is more useful between the two for Newtonian base fluids. There are several types of nanoparticles, namely, metals, oxides, carbides, nitrides, or CNTs, which are normally used. Different nanoparticle types have different impacts on the enhancement of thermal conductivity. In addition to the type, the shape of nanoparticles is equally liable to the increase of effective thermal conductivity of the mixture. Maxwell<sup>[4]</sup> proposed a model for thermal conductivity of a solid-liquid mixture and based on his model the effective thermal conductivity is given by

$$k_{\text{eff, Maxwell}} = \frac{\kappa_p + 2\kappa_1 + 2\phi(\kappa_p - \kappa_1)}{\kappa_p + 2\kappa_1 - \phi(\kappa_p - \kappa_1)} \kappa_1,$$

<sup>†</sup>Corresponding author. E-mails: [krish.math@yahoo.com](mailto:krish.math@yahoo.com); [krishmath@bhu.ac.in](mailto:krishmath@bhu.ac.in)

where  $\kappa_p$  is thermal conductivity of solid particle and  $\kappa_l$  is thermal conductivity of liquid. Maxwell's model of effective thermal conductivity is based on the assumption that the solid particles are of a spherical shape. Later, Hamilton and Crosser<sup>[5]</sup> suggested a new model for effective thermal conductivity of the mixture as

$$\kappa_{\text{eff, Ham\&Cros}} = \frac{\kappa_p + (m-1)\kappa_l - (m-1)\phi(\kappa_l - \kappa_p)}{\kappa_p + (m-1)\kappa_l + \phi(\kappa_l - \kappa_p)} \kappa_l,$$

where  $m = 3/\psi^*$  represents the shape factor,  $\psi^*$  being the sphericity which is defined as the ratio of the surface area of the sphere having same volume to that of the solid particle, to the surface area of the solid particle. So, obviously for spherical-shaped particles  $m$  is equal to 3, i.e., for  $m = 3$ , Hamilton and Crosser's model becomes Maxwell's model. Also, for some standard particle shapes, the values of  $m$  are given in Table 1. These two models are independent of size of the solid particles and it means that these two are equally valid for mixtures having nano-sized particles. One can also find some other proposed models<sup>[6,7]</sup> to describe effective thermal conductivity. Detailed analysis of thermal conductivity of nanofluid with alumina nanoparticles and ethylene glycol base fluid was reported by Beck *et al.*<sup>[8]</sup> considering various factors along with different shapes of particles. Timofeeva *et al.*<sup>[9]</sup> experimentally verified the effective thermal conductivity model by Hamilton and Crosser<sup>[5]</sup> using alumina nanoparticles and the hybrid base fluid consisting of water and ethylene glycol in 1:1 volume ratio. Later, Ellahi *et al.*<sup>[10]</sup> described the effect of different shapes of nanoparticles on entropy generation in MHD natural convection and Hamid *et al.*<sup>[11]</sup> discussed the rotating flow of nanofluid along a stretching sheet considering various shapes of  $\text{MoS}_2$  nanoparticles. Some other important investigations on nanofluid with various shapes of nanoparticles may be found in the literature.<sup>[12-17]</sup>

**Table 1.** The values of shape factor for various shapes of nanoparticles.

Shapes	Spheres	Bricks	Cylinders	Platelets	Blades
$m$	3	3.7	4.9	5.7	8.6

A porous medium can be used to achieve an adequate cooling rate, i.e., usage of porous media may be treated as a technique for heat transfer enhancement. Porous media are solid materials that have interconnecting pores or voids. So, these are open cell, rigid, and saturated, which indicates that inter-connected pores in the medium are completely filled with some fluid and that fluid may easily flow through the pores. Simultaneous use of both porous media and nanofluid is capable of grabbing substantial attention as new technique to achieve a satisfactory cooling rate with a wide range of applications. For porous media usage, the contact area between fluid and solid surface increases, whereas nanofluids cause enhancement in effective thermal conductivity of the mixture

and these increase the rate of heat transfer. The treatment of nanofluids along with porous media has various beneficial applications, such as higher heat transfer, minimum clogging, miniaturization of system, size reduction of heat transfer system, and microchannel cooling, etc. The thermal instability of nanofluid flow in porous medium was investigated by Nield and Kuznetsov<sup>[18]</sup> taking the Darcy model and Kuznetsov and Nield<sup>[19]</sup> for the Brinkman model. Ahmad and Pop<sup>[20]</sup> simultaneously considered nanofluid and porous medium for mixed convection on vertical flat plate, whereas, mixed convection on a vertical wedge was discussed by Gorla *et al.*<sup>[21]</sup> with similar consideration. Hatami and Ganji<sup>[22]</sup> took sodium alginate (SA) as a base fluid and titanium dioxide ( $\text{TiO}_2$ ) as nanoparticles to explore heat transfer characteristics for flow inside two coaxial cylinders in a porous medium. Xu *et al.*<sup>[23]</sup> discussed the forced convective nanofluid flow through foam metals in a duct and reported a pressure drop. Xu and Xing<sup>[24]</sup> numerically investigated natural convective nanofluids flow in a metal foam cavity using the lattice Boltzmann (LB) model. Convective heat transfer in nanofluid flows in foam metals was studied by Xu *et al.*<sup>[25,26]</sup> with the local thermal non-equilibrium (LTNE) effect. Later, Xu *et al.*<sup>[27]</sup> described, in detail, various modes of heat transfer for nanofluid flow in a porous medium. Mehryan *et al.*<sup>[28]</sup> illustrated the flow of magnetic hybrid nanofluid inside a double-porous medium. Recently, Roşca *et al.*<sup>[29]</sup> studied stagnation-point flow of nanofluid towards a vertical plate.

Motivated by the engineering requirement of strong cooling rate and by the fact that nanofluid and porous medium together could be able to fulfill the requirement very efficiently, here we investigate the unsteady stagnation-point flow of Cu-H<sub>2</sub>O nanofluid on a flat surface in a porous medium taking effect of various shapes of nanoparticles. Viscous dissipation and thermal radiation effects are also considered. This study will explore how the shapes of the nanoparticles play a significant role in controlling heat transfer, i.e., the cooling rate along with other physical parameters. This type of stagnation-point flow problem has many applications, like, the cooling of nuclear reactors and electronic devices, heat exchangers located in a region having small-velocity, solar pond, oil extraction and transportation, photo-catalysis, etc.

## 2. Problem formulation and basic equations

Consider the unsteady boundary layer flow near a stagnation-point in Cu-H<sub>2</sub>O nanofluid over a flat plate embedded in porous medium. The external stagnation-flow velocity is assumed to vary linearly in the form of  $u_e(x,t) = ax(1-ct)^{-1}$ , where  $a (> 0)$  and  $c$  are constants. The wall temperature  $T_w$  is assumed variable. As  $y$  attends to infinity, the value of temperature reaches to a constant value  $T_\infty$ . In addition, the viscous dissipation effect and thermal radiation are

144 considered. Under these assumptions, along with the bound-  
145 ary layer structure, the governing equations are

$$146 \quad \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \quad (1)$$

$$147 \quad \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\partial u_e}{\partial t} + u_e \frac{\partial u_e}{\partial x} \\ 148 \quad + \nu_{nf} \frac{\partial^2 u}{\partial y^2} + \frac{\nu_{nf}}{K_1} (u_e - u), \quad (2)$$

$$149 \quad \frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{\kappa_{nf}}{(\rho c_p)_{nf}} \frac{\partial^2 T}{\partial y^2} - \frac{1}{(\rho c_p)_{nf}} \frac{\partial q_r}{\partial y} \\ 150 \quad + \frac{\mu_{nf}}{(\rho c_p)_{nf}} \left( \frac{\partial u}{\partial y} \right)^2. \quad (3)$$

151 The appropriate boundary conditions are

$$152 \quad t < 0: u = 0, v = 0, T = T_w \text{ for any } x, y, \\ 153 \quad t \geq 0: u = 0, v = 0, T = T_w \text{ at } y = 0, \\ 154 \quad u \rightarrow u_e(x, t), T \rightarrow T_\infty \text{ as } y \rightarrow \infty, \quad (4)$$

155 where  $u$  and  $v$  are components of velocity along  $x$ - and  $y$ -  
156 axes, respectively,  $T$  is temperature of the nanofluid,  $K_1$   
157  $[= K_0/(1 - ct)^{-1}]$  is variable permeability of porous material  
158 with  $K_0$  being the initial value of permeability,  $q_r$  is radiative  
159 heat flux,  $\nu_{nf}$  is kinematic viscosity of the nanofluid,  $(\rho c_p)_{nf}$   
160 is heat capacity of the nanofluid,  $\kappa_{nf}$  is thermal conductivity  
161 of the nanofluid,  $\mu_{nf}$  is viscosity of nanofluid, and  $\rho_{nf}$  is the  
162 density of the nanofluid, which are defined as<sup>[30]</sup>

$$163 \quad \rho_{nf} = (1 - \phi)\rho_f + \phi\rho_s, \quad \mu_{nf} = \frac{\mu_f}{(1 - \phi)^{2.5}}, \quad \nu_{nf} = \frac{\mu_{nf}}{\rho_{nf}}, \\ 164 \quad (\rho c_p)_{nf} = (1 - \phi)(\rho c_p)_f + \phi(\rho c_p)_s, \\ 165 \quad \frac{\kappa_{nf}}{\kappa_f} = \frac{\kappa_s + (m - 1)\kappa_f - (m - 1)\phi(\kappa_f - \kappa_s)}{\kappa_s + (m - 1)\kappa_f + \phi(\kappa_f - \kappa_s)}. \quad (5)$$

166 Here,  $\phi$  is nanoparticle volume fraction,  $\kappa_f$  and  $\kappa_s$  are ther-  
167 mal conductivities of fluid and of solid nanoparticles, respec-  
168 tively,  $\mu_f$  is viscosity of base fluid,  $\rho_f$  and  $\rho_s$  are densities of  
169 the fluid and of solid nanoparticles, respectively and  $m$  is the  
170 shape factor of nanoparticles. The thermophysical properties  
171 of considered nanoparticle (Cu) and base fluid (H<sub>2</sub>O) are pre-  
172 sented in Table 2. Also, various shapes of Cu-nanoparticles  
173 are taken into account, namely, sphere-like ( $m = 3$ ), brick-like  
174 ( $m = 3.7$ ), cylinder-like ( $m = 4.9$ ), platelet-like ( $m = 5.7$ ), and  
175 blade-like ( $m = 8.6$ ).

176 The  $T_w(x, t)$  is taken in the following form:<sup>[31]</sup>

$$177 \quad T_w = T_\infty + T_0 \{ax^2/2\nu_f\} (1 - ct)^{-2}. \quad (6)$$

178 The radiative heat flux for thermal radiation given by Seddeek  
179 and Abdelmeguid<sup>[32]</sup> is

$$180 \quad q_r = -\frac{4\sigma}{3k_{nf}^*} \frac{\partial T^4}{\partial y},$$

181 where  $\sigma$  is a constant called the Stefan–Boltzman constant,  $k_{nf}^*$

182 is the Rosseland absorption coefficient of nanofluid. It is pre-  
183 sumed that the variation in temperature within the flow field  
184 is such that  $T^4$  may be expanded in a Taylor’s series. Ex-  
185 panding  $T^4$  about  $T_\infty$  and neglecting higher-order terms we  
186 get,  $T^4 \approx 4T_\infty^3 T - 3T_\infty^4$ .

187 **Table 2.** Thermophysical properties of fluid and nanoparticles (Oz-  
top and Abu-Nada<sup>[30]</sup>).

Physical properties	H <sub>2</sub> O	Cu
$C_p$ (J/kgK)	4179	385
$\rho$ (kg/m <sup>3</sup> )	997.1	8933
$k$ (W/mK)	0.613	400

188 Hence, the radiative heat flux may be rewritten as

$$189 \quad q_r = -\frac{4\sigma}{3k_{nf}^*} \frac{\partial T^4}{\partial y} = -\frac{16\sigma T_\infty^3}{3k_{nf}^*} \frac{\partial^2 T}{\partial y^2} \quad (7)$$

190 and consequently Eq. (3) reduces to

$$191 \quad \frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{\kappa_{nf}}{(\rho c_p)_{nf}} \frac{\partial^2 T}{\partial y^2} \\ 192 \quad + \frac{16\sigma T_\infty^3}{3k_{nf}^*(\rho c_p)_{nf}} \frac{\partial^2 T}{\partial y^2} + \frac{\mu_{nf}}{(\rho c_p)_{nf}} \left( \frac{\partial u}{\partial y} \right)^2. \quad (8)$$

193 The following similarity transformations are adopted to do the  
194 magic, i.e., to reduce PDEs to ODEs:

$$195 \quad \eta = \sqrt{\frac{u_e}{\nu_f x}} y, \quad \psi = \sqrt{u_e x} v_f f(\eta), \quad \theta(\eta) = \frac{T - T_\infty}{T_w - T_\infty}, \quad (9)$$

196 where  $\eta$  is the similarity variable,  $\nu_f$  is the kinematic viscos-  
197 ity of the base fluid and  $\psi$  is the stream function defined as  
198  $u = \partial\psi/\partial y$  and  $v = -\partial\psi/\partial x$ , which identically satisfies the  
199 equation of continuity (1). In view of relations in Eq. (9), we  
200 have the following transformed self-similar ordinary differen-  
201 tial equations:

$$202 \quad \frac{1}{\phi_1} f''' + f f'' - f'^2 + 1 + \frac{K}{\phi_1} (1 - f') \\ 203 \quad - A \left( f' + \frac{1}{2} \eta f'' - 1 \right) = 0, \quad (10)$$

$$204 \quad \frac{\kappa_{nf}/\kappa_f}{\phi_2} \left( 1 + \frac{4}{3} R \right) \theta'' + Pr (f \theta' - 2 f' \theta) \\ 205 \quad - A Pr \left( 2\theta + \frac{1}{2} \eta \theta' \right) + \frac{Pr E}{\phi_3} f'^2 = 0, \quad (11)$$

206 where  $K = \nu_f/K_0 a$  is the permeability parameter,  $A = c/a$   
207 is the unsteady parameter,  $Pr = \nu_f/[\kappa_f(\rho c_p)_f]$  is the Prandtl  
208 number,  $R = (4\sigma T_\infty^3)/(\kappa_{nf} k_{nf}^*)$  is the radiation parameter,  $E =$   
209  $u_e^2/[(c_p)_f(T_w - T_\infty)]$  is the Eckert number and  $\phi_1, \phi_2, \phi_3$  are  
210 given as

$$211 \quad \phi_1 = (1 - \phi)^{2.5} \left( 1 - \phi + \phi \frac{\rho_s}{\rho_f} \right), \\ 212 \quad \phi_2 = \left[ 1 - \phi + \phi \frac{(\rho c_p)_s}{(\rho c_p)_f} \right], \\ 213 \quad \phi_3 = (1 - \phi)^{2.5} \left[ 1 - \phi + \phi \frac{(\rho c_p)_s}{(\rho c_p)_f} \right]. \quad (12)$$

215 The transformed boundary conditions in (5) are

$$216 \quad f(0) = 0, \quad f'(0) = 0, \quad \theta(0) = 1, \\ 217 \quad f'(\infty) \rightarrow 1, \quad \theta(\infty) \rightarrow 0. \quad (13)$$

218 It is well known that the quantities, like skin-friction coefficient  
219  $C_{fr}$  (related to surface drag force) and local Nusselt num-  
220 ber  $Nu_x$  (related to surface heat transfer rate), which are useful  
221 and important in physical and engineering viewpoints, are di-  
222 rectly proportional to  $f''(0)$  and  $-\theta'(0)$ , respectively and their  
223 expressions look like

$$224 \quad C_{fr} Re_x^{1/2} = \frac{1}{(1-\phi)^{2.5}} f''(0), \\ 225 \quad Nu_x Re_x^{-1/2} = -\frac{\kappa_{nf}}{\kappa_f} \theta'(0), \quad (14)$$

226 where  $Re_x = u_e x / \nu_f$  is the local Reynolds number.

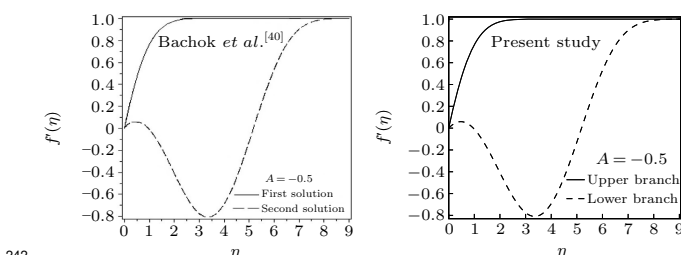
### 227 3. Solution methodology and its validation

228 The coupled nonlinear Eqs. (10) and (11) with Eq. (12)  
229 constitute a BVP and the BVP is numerically solved by a  
230 shooting method by converting it into an IVP. We are omitting  
231 details of the method,<sup>[33–39]</sup> which is already available in the  
232 literature. To confirm the accuracy of the numerical scheme  
233 and computational results, the values of  $f''(0)$  for  $\phi = 0.1$  and  
234  $K = 0$  are compared with the published results of Bachok *et al.*  
235 *al.*<sup>[40]</sup> and Salem *et al.*<sup>[41]</sup> in Table 3 and the results are found  
236 in brilliant agreement. In addition, a graphical comparison of  
237 velocity profiles for  $A = -0.5$  with  $\phi = 0$  and  $K = 0$  with the  
238 results of Bachok *et al.*<sup>[40]</sup> is performed in Fig. 1 and those  
239 profiles are observed to have an excellent match.

240 **Table 3.** Comparison of the values of  $f''(0)$  for different values of  $A$  with  
 $\phi = 0.1$  and  $K = 0$ .

$A$	Bachok <i>et al.</i> <sup>[40]</sup>	Salem <i>et al.</i> <sup>[41]</sup>	Present study
1	1.7604	1.7603982	1.760417
-1	1.0845	1.0845304	1.084530
	[-1.1573]	[-1.1572880]	[-1.157300]
-2	0.6499	0.6498771	0.649877
	[-1.9885]	[-1.9885181]	[-1.988516]
-3	0.1045	0.1044666	0.104469
	[-2.3251]	[-2.3251486]	[-2.325146]
-4	-0.6757	-0.67567808	-0.675672
	[-2.2646]	[-2.2646440]	[-2.264642]

[ ] Values for the lower branch solution.

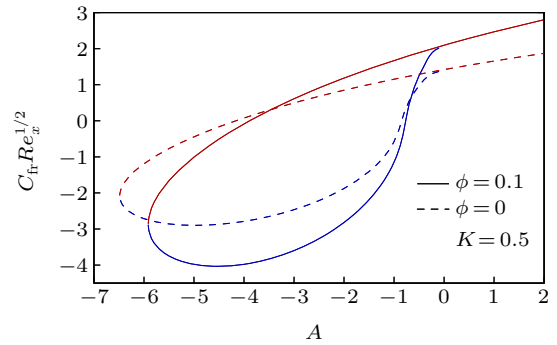


243 **Fig. 1.** Comparison of velocity profiles for  $A = -0.5$  with  $\phi = 0$  and  $K = 0$ .

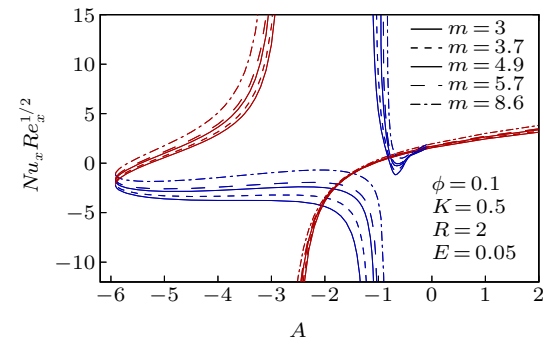
### 244 4. Results and discussion

245 To know the impact of nanoparticles and its various  
246 shapes in controlling heat transfer in the unsteady stagnation-  
247 point flow of Cu–H<sub>2</sub>O nanofluid on a flat surface in a porous  
248 medium, the numerically computed results of various physi-  
249 cal properties are presented in Figs. 2–18 for different values  
250 of involved parameters, namely, the unsteady parameter ( $A$ ),  
251 nanoparticle volume fraction ( $\phi$ ), shape factor of nanoparticles  
252 ( $m$ ), permeability parameter ( $K$ ), radiation parameter ( $R$ ), and  
253 the Eckert number ( $E$ ) with the Prandtl number being taken  
254 as 6.13 (water) throughout the computations. The volume  
255 fraction of nanoparticles is considered 0 and 0.1, where  $\phi = 0$   
256 represents the water without any nanoparticle. Results for  
257 skin friction coefficient and the Nusselt number demonstrate  
258 the existence of dual solutions for any value of decelerating  
259 unsteady parameter ( $A < 0$ ). But the dual solutions exist up to  
260 a certain critical value (say,  $A_c < 0$ ) of decelerating unsteady  
261 parameter and beyond that critical value ( $A < A_c$ ) there is no  
262 self-similar solution. Whereas, for accelerating unsteady and  
263 steady cases ( $A \geq 0$ ), the solution is single, i.e., unique. Due  
264 to decelerating unsteadiness of the flow dual solutions exist.  
265 The negative value of the unsteady parameter means that the  
266 constant  $c$  takes a negative value and it is the coefficient of  
267 the time variable. It consequently implies that for decelerat-  
268 ing unsteadiness, the impact of the time variable on the flow  
269 dynamics is completely opposite and it creates a situation of  
270 uncertainty as time progresses. Therefore, dual solutions of  
271 the flow dynamics are witnessed for decelerating unsteadiness.  
272 On the other hand, the presence of nanoparticles only  
273 does not affect the critical value,  $A_c$ ,<sup>[40]</sup> but if the medium  
274 of flow is a porous medium, then the nanoparticles' presence  
275 disturbs the critical value for the existence of dual solutions  
276 and so we can accept this as an important finding of the inves-  
277 tigation. When the nanoparticle volume fraction is 0.1 then  
278 critical value  $A_c$  is  $-5.9135$  for  $K = 0.5$  and when  $\phi = 0$ ,  $A_c$   
279 is  $-6.4843$  for  $K = 0.5$  (Fig. 2). It directly means that in a  
280 porous medium the nanoparticles cause the reduction in the  
281 magnitude of  $A_c$ , i.e., the range of existence of dual solutions  
282 reduces when nanoparticles are added to the flow field. It is  
283 also worth noting that the shapes of nanoparticles have no  
284 impact on the aforesaid existence range of dual solutions. In  
285 addition, for a unique solution and upper branch solution the  
286 drag force enhances due to the presence of nanoparticles for  
287 accelerating the unsteady parameter and some cases of decel-  
288 erating the unsteady parameter. While in the lower branch  
289 solution the drag force reduces due to nanoparticles for all  
290 values of decelerating the unsteady parameter except near the  
291 zero value. Restriction on the surface drag force is very crucial  
292 in application viewpoints because the drag force is imposed  
293 on the solid surface. In Fig. 3, the Nusselt number is plotted

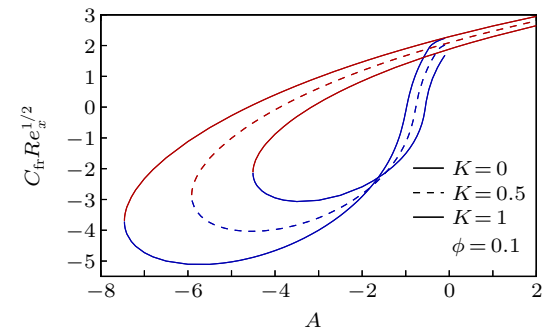
294 for different shapes of Cu-nanoparticles, i.e., different values  
 295 of shape factor  $m$  and it is witnessed that as  $m$  increases  
 296 the Nusselt number also increases, i.e., the cooling rate en-  
 297 hances with  $m$ . The shape factor is inversely proportional to  
 298 the sphericity, i.e., the ratio of the surface area of the sphere  
 299 having equal volume to that of nanoparticle, to the surface area  
 300 of the nanoparticle. So, as  $m$  increases, sphericity decreases,  
 301 i.e., the surface of the nanoparticle is large and hence the  
 302 heat-carrying capacity of the nanoparticle becomes higher. As  
 303 a consequence, the cooling rate is higher when  $m$  has larger  
 304 values. So, the nanoparticles in the form of blades are the  
 305 best for the heat transfer nanofluid when it is compared with  
 306 the other shapes (spheres, bricks, cylinders, and platelets) of  
 307 nanoparticles. Therefore, in many engineering and industrial  
 308 processes related to heat transfer, blade shape nanoparticles  
 309 are more beneficial than other shapes considered and so, the  
 310 shape of nanoparticles can control the heat transfer and hence  
 311 the final quality of the product. The permeability of the porous  
 312 medium has a strong influence on the existence range of dual  
 313 solutions, i.e., on the critical value,  $A_c$  (Fig. 4). The range  
 314 of existence of dual solutions is wider when the permeability  
 315 parameter is larger. The values of  $A_c$  are  $-4.5066$ ,  $-5.9135$ ,  
 316 and  $-7.4581$  for  $K = 0$ ,  $K = 0.5$ , and  $K = 1$ . The permeabil-  
 317 ity parameter is inversely proportional to the permeability of  
 318 porous material. So, as  $K$  increases the permeability of porous  
 319 medium becomes less, i.e., the Darcy resistive force due to  
 320 porous medium is larger and it results in a significant aug-  
 321 mentation of the range of existence of dual solutions. For the  
 322 same reason, the drag force, i.e., the skin friction coefficient is  
 323 noticeably high with the permeability parameter in the upper  
 324 branch solution and unique solution. For different values of  
 325  $K$ , the Nusselt number is plotted for all considered values of  
 326 shape factor  $m$ , i.e., for various shapes of Cu-nanoparticles in  
 327 Fig. 5. For the upper branch solution, the Nusselt number,  
 328 i.e., the cooling rate rises with  $K$  for all shapes of consid-  
 329 ered Cu-nanoparticles and physically, it is the consequence of  
 330 less permeability of the porous medium. For less a perme-  
 331 able porous medium, i.e., for a more compact porous medium  
 332 though momentum transport obstructed, but it is quite suitable  
 333 for high heat transport. So, this very high heat transfer rate  
 334 due to porous medium in the nanofluid flow has colossal appli-  
 335 cations in many industrial and engineering problems, like the  
 336 cooling of electronic devices, the cooling of metallic sheets,  
 337 etc., while in the lower branch the contrasting effect is wit-  
 338 nessed. The impact of the radiation parameter and the Eckert  
 339 number on the cooling rate, i.e. the Nusselt number, are depic-  
 340 ted in Figs. 6 and 7, respectively. The cooling rate is higher  
 341 for larger values of the radiation parameter. It implies that as  
 342 the thermal radiation level is high the cooling rate raises and  
 343 physically this is the expected outcome. Whereas, a non-zero  
 344 Eckert number cooling rate slightly reduces for many cases of



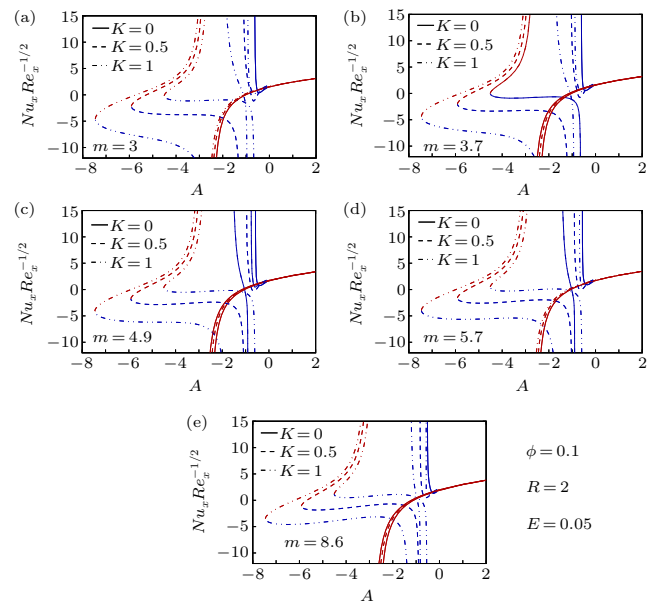
347 **Fig. 2.** Skin-friction coefficient,  $C_{fr}Re_x^{1/2}$  with  $A$  for different nanoparticle volume fractions.



349 **Fig. 3.** Nusselt number,  $Nu_x Re_x^{-1/2}$  with  $A$  for different shapes of nanoparticles.

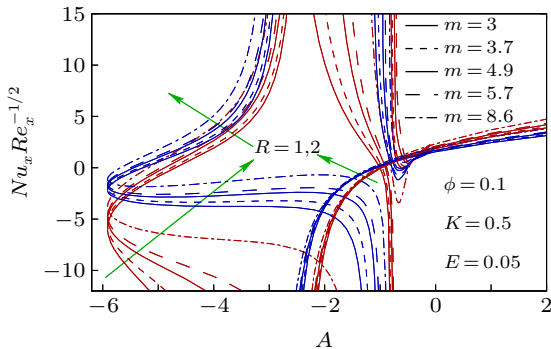


351 **Fig. 4.** Skin-friction coefficient,  $C_{fr}Re_x^{1/2}$  with  $A$  for different values of  $K$ .

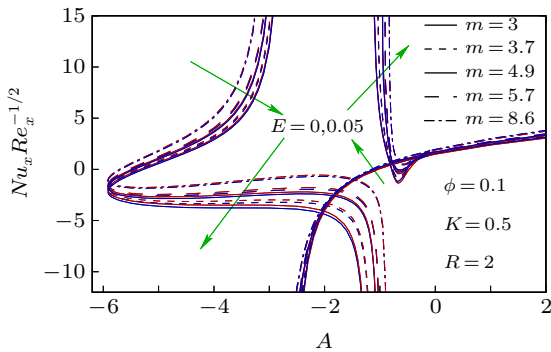


353 **Fig. 5.** Nusselt number,  $Nu_x Re_x^{-1/2}$  with  $A$  for different values of  $K$ .

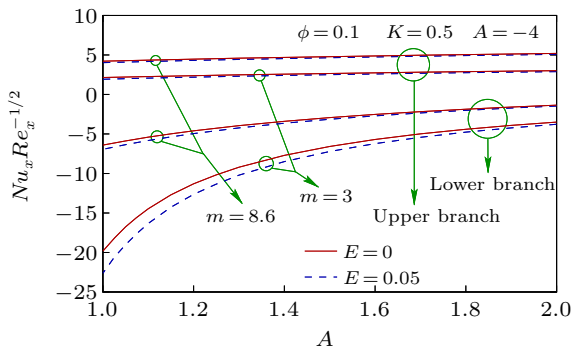
354 decelerating unsteady flow and for accelerating unsteady flow  
 355 a minute enhancement in cooling rate is observed. Moreover,  
 356 in Fig. 8 the Nusselt number is plotted with  $R$  for different  $E$   
 357 and  $m$ . It reveals that the effect of the Eckert number on heat  
 358 transfer coefficient is less prominent with the rise of radiation  
 359 and the radiation has a considerable impact on heat transfer  
 360 for different-shaped nanoparticles. Radiative heat transfer is  
 361 very effective, like convective heat transfer in the presence of  
 362 nanoparticles.



363  
 364 **Fig. 6.** Nusselt number,  $Nu_x Re_x^{-1/2}$  with  $A$  for different values of  $R$ .



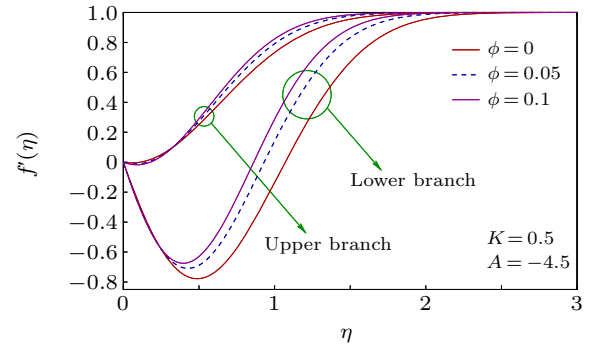
365  
 366 **Fig. 7.** Nusselt number,  $Nu_x Re_x^{-1/2}$  with  $A$  for different values of  $E$ .



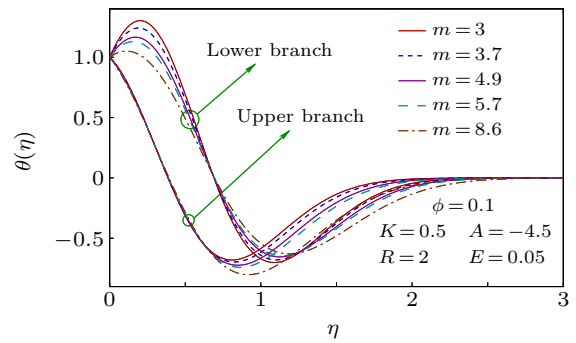
367  
 368 **Fig. 8.** Nusselt number  $Nu_x Re_x^{-1/2}$  with  $R$  for different values of  $E$ .

369 For different values of Cu-nanoparticle volume fraction  
 370  $\phi$ , the velocity profiles are shown in Fig. 9. For both solu-  
 371 tion branches, in spite of initial decay in velocity the boundary  
 372 layer thickness (BLT) is reduced with  $\phi$ . Due to the nanopar-  
 373 ticle presence the intermolecular force increases and as a con-  
 374 sequence, the free stream velocity is achieved earlier and it  
 375 causes the decline of BLT. In Fig. 10, the temperature profile

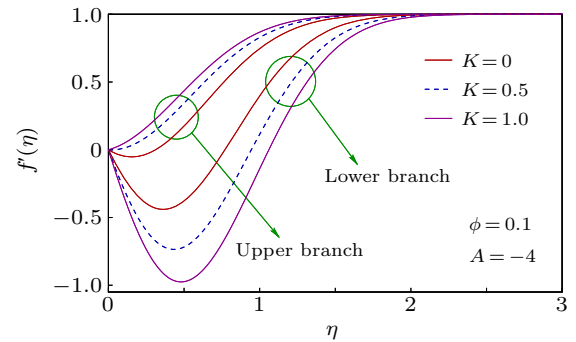
376  $\theta(\eta)$  is plotted for all considered values of shape factor  $m$ .  
 377 It exhibits an early decrease of temperature and an increased  
 378 thermal BLT with  $m$ . In reality, the high heat transfer rate with  
 379 larger  $m$  (due to larger surface area) affects free stream temper-  
 380 ature up to a longer distance from the flat surface and therefore  
 381 thermal BLT becomes thick.



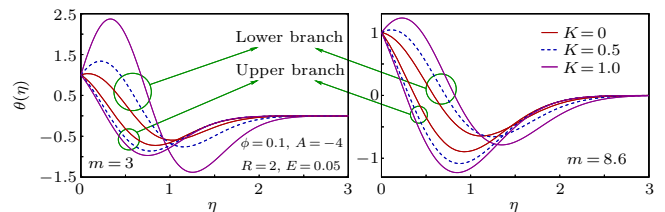
382  
 383 **Fig. 9.** Velocity profiles for different nanoparticle volume fractions.



384  
 385 **Fig. 10.** Temperature profiles for different shapes of nanoparticles.



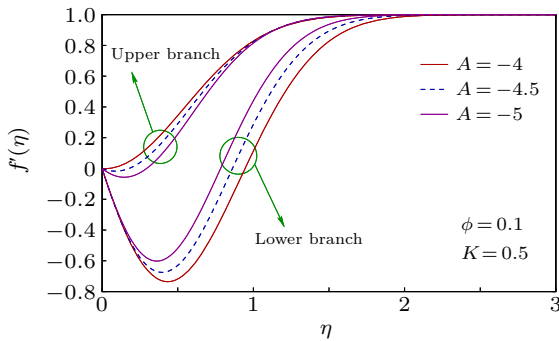
386  
 387 **Fig. 11.** Velocity profiles for different  $K$ .



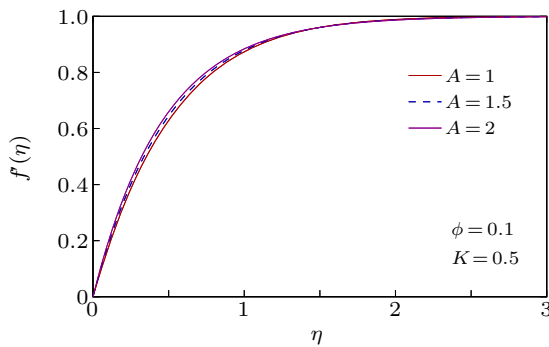
388  
 389 **Fig. 12.** Temperature profiles for different  $K$ .

390 The impact of permeability parameter  $K$  (related to the  
 391 permeability of the porous medium) on the nanofluid velocity  
 392 and temperature profiles are illustrated in Figs. 11 and 12. It  
 393 exhibits contrasting effects on two solution branches. In the

394 upper branch solution, the velocity rises with  $K$  and BLT turns  
 395 out to be thinner. The Darcy resistive force in porous medium  
 396 is inversely proportional to its permeability and therefore, with  
 397 the rise of  $K$ , i.e., and with a medium having less permeabil-  
 398 ity, this force grows. Consequently, a shrink of BLT occurs.  
 399 Whereas the temperature (plotted for two values of  $m$ ) inside  
 400 the boundary layer shows a decay with  $K$  in the upper branch  
 401 and lower branch temperature exhibits an initial rise, while  
 402 away from the surface, the reverse result is found.

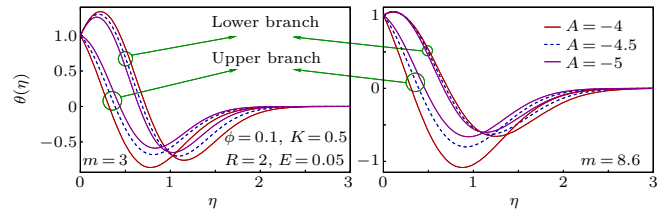


403 **Fig. 13.** Velocity profiles for different  $A (< 0, \text{decelerating unsteady flow})$ .

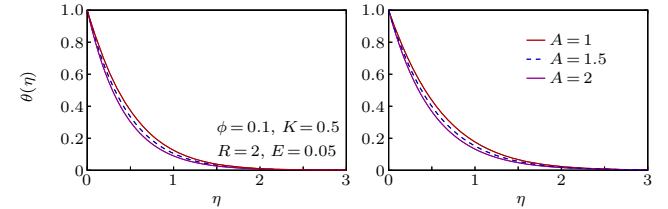


405 **Fig. 14.** Velocity profiles for different  $A (> 0, \text{accelerating unsteady flow})$ .

407 The nanofluid velocity profiles are displayed in Figs. 13  
 408 and 14 for decelerating and accelerating unsteady flows. Due  
 409 to increasing magnitude of decelerating unsteady parameter  
 410 ( $A < 0$ ), the flow velocity reduces in the upper branch so-  
 411 lution and it increases with accelerating unsteady parameter  
 412 ( $A > 0$ ). Decelerating unsteadiness of the flow creates such a  
 413 situation, for which dual solutions exist and no other param-  
 414 eter can control this uncertain situation of the flow. It is already  
 415 witnessed that the Darcy force of porous medium increases the  
 416 region of uncertainty of dual solutions. Whereas accelerating  
 417 unsteadiness is natural and has no ambiguous property, like  
 418 decelerating unsteadiness and consequently, the solution be-  
 419 comes unique. In Figs. 15 and 16, the nanofluid temperature  
 420 profiles are presented for various values of  $A$ . For decelerating  
 421 unsteady flow, the temperature rises with increasing magni-  
 422 tude of  $A$  in the upper branch with thermal BLT being thinner  
 423 and though the initial behavior is the opposite for the lower  
 424 branch, thermal BLT reduces with a magnitude of  $A$ . Whereas  
 425 the nanofluid temperature decreases with  $A$  in unique solution  
 426 for accelerating unsteady flow.

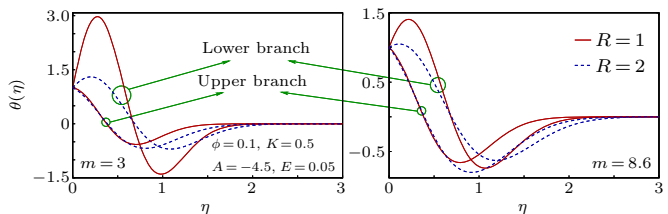


427 **Fig. 15.** Temperature profiles for different  $A (> 0, \text{decelerating unsteady flow})$ .

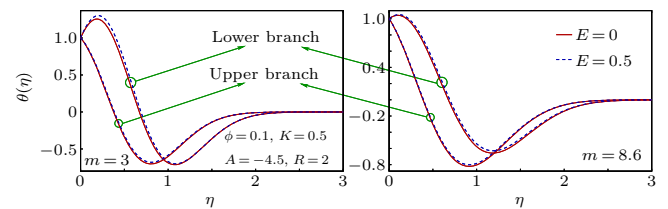


429 **Fig. 16.** Temperature profiles for different  $A (> 0, \text{accelerating unsteady flow})$ .

431 The nanofluid temperature profiles are depicted in  
 432 Figs. 17 and 18 for different values of the radiation param-  
 433 eter and the Eckert number, respectively. For thermal radiation,  
 434 the thermal BLT is expanded and it takes place because the radi-  
 435 ative heat transfer disturbs the temperature in a free stream  
 436 for a longer distance from the flat surface. The growth of ther-  
 437 mal BLT is meaningfully large for blade-nanoparticles and so  
 438 this thermal BLT expansion due to radiation is crucial in sev-  
 439 eral engineering processes, like seawater desalination, solar  
 440 thermal chemical reaction and combustor,<sup>[27]</sup> when the choice  
 441 of shape of the nanoparticles is made. For growth in the Eck-  
 442 ert number, the temperature inside nanofluid boundary layer  
 443 shows an increasing trend.



444 **Fig. 17.** Temperature profiles for different  $R$ .



447 **Fig. 18.** Temperature profiles for different  $E$ .

### 449 5. Stability analysis of obtained solutions

450 Due to the existence of dual solutions for a specific range  
 451 of unsteady parameter (for decelerating unsteady flow) along  
 452 with a unique solution (for steady and accelerating unsteady  
 453 flow), it becomes necessary to check the stability of those so-  
 454 lutions. So, a stability analysis is performed following Weid-

man *et al.*<sup>[42]</sup> and Bakar *et al.*<sup>[43]</sup> A new dimensionless similarity variable  $\tau$  is introduced and the similarity solutions are taken as

$$\begin{aligned} \psi &= \sqrt{x\nu_f}u_e F(\eta, \tau), \\ T &= T_\infty + (T_w - T_\infty)\Phi(\eta, \tau), \\ \eta &= \sqrt{\frac{u_e}{x\nu_f}}y, \\ \tau &= \frac{u_e t}{x}. \end{aligned} \tag{15}$$

Using Eq. (15), Eqs. (2) and (3) with Eq. (4) reduce to

$$\begin{aligned} \frac{1}{\phi_1} \frac{\partial^3 F}{\partial \eta^3} + F \frac{\partial^2 F}{\partial \eta^2} - \left(\frac{\partial F}{\partial \eta}\right)^2 + 1 + \frac{K}{\phi_1} \left(1 - \frac{\partial F}{\partial \eta}\right) \\ - A \left(\frac{\partial F}{\partial \eta} + \frac{\eta}{2} \frac{\partial^2 F}{\partial \eta^2} - 1 + \tau \frac{\partial^2 F}{\partial \tau \partial \eta}\right) - \frac{\partial^2 F}{\partial \tau \partial \eta} = 0, \end{aligned} \tag{16}$$

$$\begin{aligned} \frac{\kappa_{nf}/\kappa_f}{\phi_2} \left(1 + \frac{4}{3}R\right) \frac{\partial^2 \Theta}{\partial \eta^2} + Pr \left(F \frac{\partial \Theta}{\partial \eta} - \frac{\partial \Theta}{\partial \tau}\right) \\ - APr \left(\frac{\eta}{2} \frac{\partial \Theta}{\partial \eta} + \tau \frac{\partial \Theta}{\partial \tau}\right) + \frac{PrE^*}{\phi_3} \left(\frac{\partial^2 F}{\partial \eta^2}\right)^2 = 0 \end{aligned} \tag{17}$$

with

$$\begin{aligned} F(0, \tau) = 0, \quad F'(0, \tau) = 0, \quad \Theta(0, \tau) = 1, \\ F'(\eta, \tau) \rightarrow 1, \quad \Theta(\eta, \tau) \rightarrow 0 \quad \text{as } \eta \rightarrow \infty. \end{aligned} \tag{18}$$

In order to test the stability of solutions  $f(\eta)$ ,  $\theta(\eta)$  satisfying the BVP (10), (11), and (13), the following are introduced (Weidman *et al.*<sup>[42]</sup>):

$$\begin{aligned} F(\eta, \tau) = f(\eta) + e^{-\gamma\tau} f^*(\eta, \tau), \\ \Theta(\eta, \tau) = \theta(\eta) + e^{-\gamma\tau} \theta^*(\eta, \tau), \end{aligned} \tag{19}$$

where  $f^*(\eta, \tau)$ ,  $\theta^*(\eta, \tau)$  are disturbances to solutions  $f(\eta)$ ,  $\theta(\eta)$  and are assumed very small in comparison with the solutions and  $\gamma$  is rate of disturbance. Using Eq. (19) in Eqs. (16)–(18) and linearizing we have

$$\begin{aligned} \frac{1}{\phi_1} \frac{\partial^3 f^*}{\partial \eta^3} + f \frac{\partial^2 f^*}{\partial \eta^2} + f^* \frac{d^2 f}{d\eta^2} - 2 \frac{df}{d\eta} \frac{\partial f^*}{\partial \eta} \\ - A \left(\frac{\partial f^*}{\partial \eta} + \frac{\eta}{2} \frac{\partial^2 f^*}{\partial \eta^2} + \tau \frac{\partial^2 f^*}{\partial \tau \partial \eta} - \gamma\tau \frac{\partial f^*}{\partial \eta}\right) \\ - \frac{K}{\phi_1} \frac{\partial f^*}{\partial \eta} - \frac{\partial^2 f^*}{\partial \tau \partial \eta} + \gamma \frac{\partial f^*}{\partial \eta} = 0, \end{aligned} \tag{20}$$

$$\begin{aligned} \frac{\kappa_{nf}/\kappa_f}{\phi_2} \frac{\partial^2 \theta^*}{\partial \eta^2} + Pr \left(f \frac{\partial \theta^*}{\partial \eta} + f^* \frac{d\theta}{d\eta} - \frac{\partial \theta^*}{\partial \tau} + \gamma\theta^*\right) \\ - APr \left(\frac{\eta}{2} \frac{\partial \theta^*}{\partial \eta} + \tau \frac{\partial \theta^*}{\partial \tau} - \tau\gamma\theta^*\right) \\ + \frac{2PrE^*}{\phi_3} \frac{d^2 f}{d\eta^2} \frac{\partial^2 f^*}{\partial \eta^2} = 0 \end{aligned} \tag{21}$$

subject to

$$f^*(0, \tau) = 0, \quad \frac{\partial f^*}{\partial \eta}(0, \tau) = 0, \quad \theta^*(0, \tau) = 0,$$

$$\frac{\partial f^*}{\partial \eta}(\infty, \tau) \rightarrow 0, \quad \theta^*(\infty, \tau) \rightarrow 0. \tag{22}$$

Now, taking  $\tau = 0$  and putting  $f^*(\eta, \tau) = f_0^*(\eta)$  and  $\theta^*(\eta, \tau) = \theta_0^*(\eta)$ ,  $f_0^*(\eta)$  and  $\theta_0^*(\eta)$  being the initial disturbances to solutions, Eqs. (20)–(22) become

$$\begin{aligned} \frac{1}{\phi_1} \frac{d^3 f_0^*}{d\eta^3} + f \frac{d^2 f_0^*}{d\eta^2} + f_0^* \frac{d^2 f}{d\eta^2} - 2 \frac{df}{d\eta} \frac{df_0^*}{d\eta} \\ - A \left(\frac{df_0^*}{d\eta} + \frac{\eta}{2} \frac{d^2 f_0^*}{d\eta^2}\right) - \frac{K}{\phi_1} \frac{df_0^*}{d\eta} + \gamma \frac{df_0^*}{d\eta} = 0, \end{aligned} \tag{23}$$

$$\begin{aligned} \frac{\kappa_{nf}/\kappa_f}{\phi_2} \frac{d^2 \theta_0^*}{d\eta^2} + Pr \left(f \frac{d\theta_0^*}{d\eta} + f_0^* \frac{d\theta}{d\eta} + \gamma\theta_0^*\right) \\ - \frac{\eta APr}{2} \frac{d\theta_0^*}{d\eta} + \frac{2PrE^*}{\phi_3} \frac{d^2 f}{d\eta^2} \frac{d^2 f_0^*}{d\eta^2} = 0 \end{aligned} \tag{24}$$

with

$$f_0^*(0) = 0, \quad \frac{df_0^*}{d\eta}(0) = 0, \quad \theta_0^*(0) = 0,$$

$$\frac{df_0^*}{d\eta}(\infty) \rightarrow 0, \quad \theta_0^*(\infty) \rightarrow 0. \tag{25}$$

Equations (23) and (24) with Eq. (25) constitute an eigenvalue problem with  $\gamma$  an eigenvalue, to be determined. An infinite set of eigenvalues  $\gamma_1 < \gamma_2 < \gamma_3 < \dots$  will be obtained on solving the eigenvalue problem (23)–(25). The least eigenvalue  $\gamma_1$  will regulate the stability of the solutions  $f(\eta)$  and  $\theta(\eta)$ . If  $\gamma_1$  has a positive value, then there will be an initial decay of disturbances to the solutions and in this case, the solutions will be stable. Now, if  $\gamma_1$  has a negative value, then there is a clear indication of initial growth of disturbances to the solutions and hence the solutions will be unstable.

After solving the above eigenvalue problem, the smallest eigenvalues  $\gamma_1$  are listed in Table 4 for upper and lower branch solutions ( $A_c \leq A < 0$ , decelerating unsteady flow) and the unique solution ( $A \geq 0$ , steady and accelerating unsteady flow) for some values of  $A$  with  $\phi = 0.1$  and  $K = 0.5$ . The values of  $\gamma_1$  for the upper branch solution and the unique solution are found to be positive, while for the lower branch solution its value is negative. So, from the aforesaid analysis, it may be resolved that the upper branch and unique solutions are stable solutions, whereas the lower branch solution is an unstable solution. The stability or instability of solutions is not able to guarantee its physical existence or non-existence in real experiments. If an experiment is performed, then there will be two possibilities for decelerating unsteady flow ( $0 > A \geq A_c$ ). There may be a real and visible boundary layer flow or no boundary layer formulation in the flow field. It means that when a stable solution occurs, it will be real and visible and when an unstable solution arises, it will have no physical existence, i.e., due to many unavoidable disturbances during the experiment it will not be physically realizable. So, we may say that both solutions have physical meaning and relevance.



**Table 4.** Smallest eigenvalue,  $\gamma_1$  for some values of  $A$  with  $\phi = 0.1$  and  $K = 0.5$ .

$A$	$\gamma_1$
2	4.9075918
1	3.8994496
0	3.5090404
-1	3.14072230
-2	2.7633561
-3	2.3554984
-4	1.8871452
-5	1.2872198
-5.5	0.8583381
-5.8	0.4457369
-5.9	0.1526771
-5.91	0.0777469
-5.913	0.0301721

[ ] Values for the lower branch solution.

## 6. Concluding remarks

The unsteady stagnation-point flow of Cu–H<sub>2</sub>O nanofluid on a flat surface in a porous medium is investigated taking effects of various shapes of Cu-nanoparticles. The effects of viscous dissipation and thermal radiation are taken into consideration. The governing equations of the problem are converted into self-similar coupled ODEs which constitute a BVP and it is solved by a shooting method. After a complete analysis, a summary of findings is as follows:

- (i) Dual solutions exist for any value of the decelerating unsteady parameter ( $A < 0$ ), i.e., decelerating unsteady flow and these solutions exist up to a certain critical value  $A_c$  ( $< 0$ ). Whereas, for accelerating unsteady and steady flows ( $A \geq 0$ ), the solution is unique.
- (ii) Only the presence of nanoparticles does not affect the value of  $A_c$ , but when flow is considered in a porous medium then the magnitude of  $A_c$  decreases with nanoparticle volume fraction. Also, due to larger permeability parameter, the range of existence of dual solutions is longer.
- (iii) The shapes of nanoparticles have no influence on the value of  $A_c$ , but it has a huge impact on surface heat transfer.
- (iv) The Nusselt number, i.e., the cooling rate enhances with increasing values of shape factor  $m$  and the presence of

thermal radiation. Also, for upper branch and unique solutions, the drag force and cooling rate rise with  $K$ .

- (v) For the positive Eckert number, a minor reduction in the cooling rate is observed in some cases of decelerating unsteady flow and for the accelerating unsteady flow a contrasting effect is found.
- (vi) For the upper branch solution, the velocity rises with  $K$  along with a reduction in BLT and the opposite nature exhibits for the lower branch. Whereas, despite an initial decay of temperature, the thermal BLT enhances with  $m$ .
- (vii) For decelerating unsteady flow ( $A < 0$ ), velocity reduces in the upper branch and it increases for accelerating unsteady flow ( $A > 0$ ). Opposite trends are observed in temperature.
- (viii) After the stability analysis, it is obtained that the upper branch and unique solutions are stable, whereas the lower branch solution is unstable.

## References

- [1] Choi S U S 1995 *In: D.A. Siginer and H.P. Wang, Eds., Developments and Applications of Non-Newtonian Flows, ASME, New York* **66** 99
- [2] Buongiorno J 2006 *ASME J. Heat Transf.* **128** 240
- [3] Tiwari R K and Das M K 2007 *Int. J. Heat Mass Transf.* **50** 2002
- [4] Maxwell J C 1881 *A Treatise on Electricity and Magnetism* (2nd edn.) (Oxford: Clarendon Press) UK
- [5] Hamilton R L and Crosser O K 1962 *Ind. Eng. Chem. Fundam.* **1** 187
- [6] Yu W and Choi S U S 2003 *J. Nanoparticle Res.* **5** 167
- [7] Jang S P and Choi S U S 2004 *Appl. Phys. Lett.* **84** 4316
- [8] Beck M P, Sun T F and Teja A S 2007 *Fluid Phase Equilib.* **260** 275
- [9] Timofeeva E V, Routbort J L and Singh D 2009 *J. Appl. Phys.* **106** 014304
- [10] Ellahi R, Hassan M and Zeeshan A 2015 *Int. J. Heat Mass Transf.* **81** 449
- [11] Hamid M, Usman M, Zubair T, Ul Haq R and Wang W 2018 *Int. J. Heat Mass Transf.* **124** 706
- [12] Akbar N S, Butt A W and Tripathi D 2017 *Res. Phys.* **7** 2477
- [13] Dogonchi A S, Waqas M, Seyyedi S M, Tilehnoee M H and Ganji D D 2019 *Int. J. Heat Mass Transf.* **132** 473
- [14] Dogonchi A S, Tilehnoee M H, Waqas M, Seyyedi S M, Animasaun I L and Ganji D D 2020 *Physica A* **540** 123034
- [15] Hosseinzadeh K, Roghani S, Asadi A, Mogharrebi A and Ganji D D 2021 *Int. J. Numer. Methods Heat Fluid Flow* **31** 402
- [16] Tlili I, Samrat S P, Sandeep N and Nabwey H A 2021 *Ain Shams Eng. J.* **12** 935
- [17] Iftikhar N, Rehman A and Sadaf H 2021 *Int. Commun. Heat Mass Transf.* **120** 105012
- [18] Nield D A and Kuznetsov A V 2009 *Int. J. Heat Mass Transf.* **52** 5796
- [19] Kuznetsov A V and Nield D A 2010 *Transp. Porous Media* **81** 409
- [20] Ahmad S and Pop I 2010 *Int. Commun. Heat Mass Transf.* **37** 987
- [21] Gorla R S R, Chamkha A J and Rashad A M 2011 *Nanoscale Res. Lett.* **6** 207
- [22] Hatami M and Ganji D D 2013 *J. Mol. Liq.* **188** 155
- [23] Xu H, Gong L, Huang S and Xu M 2015 *Int. J. Heat Mass Transf.* **83** 399
- [24] Xu H and Xing Z 2017 *Int. Commun. Heat Mass Transf.* **89** 73
- [25] Xu H, Xing Z and Vafai K 2019 *Int. J. Heat Fluid Flow* **77** 242
- [26] Xu H, Xing Z B and Ghahremannezhad A 2019 *J. Porous Media* **22** 1553
- [27] Xu H J, Xing Z B, Wang F Q and Cheng Z M 2019 *Chem. Eng. Sci.* **195** 462

- 616 [28] Mehryan S A M, Sheremet M A, Soltani M and Izadi M 2019 *J. Mol. Liq.* **277** 959  
617  
618 [29] Roşca A V, Roşca N C and Pop I 2021 *Int. J. Numer. Methods Heat Fluid Flow* **31** 75  
619  
620 [30] Oztop H F and Abu-Nada E 2008 *Int. J. Heat Fluid Flow* **29** 1326  
621 [31] El-Aziz M A 2014 *J. Egypt. Math. Soc.* **22** 529  
622 [32] Seddeek M A and Abdelmeguid M S 2006 *Phys. Lett. A* **348** 172  
623 [33] Seth G S, Singha A K, Mandal M S, Banerjee A and Bhattacharyya K 2017 *Int. J. Mech. Sci.* **134** 98  
624  
625 [34] Mukhopadhyay S and Mandal I C 2014 *Chin. Phys. B* **23** 044702  
626 [35] Bhattacharyya K and Pop I 2014 *Chin. Phys. B* **23** 024701  
627 [36] Mukhopadhyay S 2014 *Chin. Phys. B* **23** 014702  
628 [37] Bhattacharyya K, Hayat T and Alsaedi A 2014 *Chin. Phys. B* **23** 124701  
629  
630 [38] Bhattacharyya K 2011 *Chin. Phys. Lett.* **28** 084702  
631 [39] Pandey A K, Rajput S, Bhattacharyya K and Sibanda P 2021 *Pramana-J. Phys.* **95** 5  
632  
633 [40] Bachok N, Ishak A and Pop I 2012 *Int. J. Heat Mass Transf.* **55** 6499  
634 [41] Salem A M, Ismai G and Fathy R 2015 *Eur. Phys. J. Plus* **130** 113  
635 [42] Weidman P D, Kubitschek D G and Davis A M J 2006 *Int. J. Eng. Sci.* **44** 730  
636  
637 [43] Bakar A, Arifin N M, Ali M F, Bachok N, Nazar R and Pop I 2018 *Appl. Sci.* **8** 483  
638